Characterisation of the velocity distribution on rigid in-vitro upper airway replicas

Annemie Van Hirtum\textsuperscript{a}, Xavier Grandchamp\textsuperscript{a}, David Marx\textsuperscript{b}, Xavier Pelorson\textsuperscript{a} and Helène Bailliet\textsuperscript{b}

\textsuperscript{a}Département Parole & Cognition, GIPSA-lab, 46, avenue Félix Viallet, 38031 Grenoble Cedex, France
\textsuperscript{b}Laboratoire d’Etudes Aerodynamiques - CNRS, Bat K, 40 avenue du recteur Pineau, 86022 Poitiers, France

annemie.vanhirtum@gipsa-lab.inpg.fr
Qualitative and quantitative characterisation of the velocity distribution is an important aspect in order to study human speech production. Classical physical phonation models exploit quasi one-dimensional flow descriptions for which the velocity distribution is obtained from an analytical relationship depending on volume airflow velocity, geometry and pressure distribution. Therefore, ‘in-vitro’ validation and characterisation of simplified flow models is obtained straightforwardly by measuring the relevant quantities. More detailed and quantitative velocity predictions on the other hand, aiming e.g. to improve phonation modelling or to study turbulent sound production, require increased precision of the qualitative and quantitative characterisation of both the mean and fluctuating part of the velocity field. The current paper presents preliminary ‘in-vitro’ measurements of the velocity distribution obtained by hot film single sensor anemometry and two component Particle Image Velocimetry. Simplified rigid geometries are assessed in order to represent different geometries encountered in the upper airways. Besides qualitative results a first quantitative comparison between simulated and measured velocities is provided and discussed in case of round free jet development.

1 Introduction

Physical modelling of speech production is mostly dealing with phonation or voiced sound production denoting sounds involving auto-oscillations of the vocal folds due to the interaction with respiratory airflow as is the case for vowels. In general simplified models are preferred for physical phonation modelling in order to establish an unambiguous relationship between model parameters and ‘in-vivo’ or ‘in-vitro’ measurable quantities. Consequently, phonation models as the classical two mass model exploit quasi one-dimensional flow descriptions in order to estimate the pressure forces exerted on the vocal folds tissues [6]. These simplified flow models provide an analytical relationship between velocity distribution, volume airflow velocity, geometry and pressure distribution [2]. Therefore validation of the quasi one-dimensional flow models is obtained straightforwardly by measuring the relevant quantities [6, 2].

Although phonation involves a major part of human sound production, vocal folds auto-oscillations are a very particular and well localised sound source. Hence, a major part of fluid flow related phenomena and associated sounds are left untreated in classical studies dealing with physical phonation modelling. Moreover, the fluid flow through the upper airways is likely to become turbulent depending on flow and articulator conditions as illustrated in Figure 1. Consequently more detailed and characterisation of the smooth flow evolution associated with the main convective flow, the onset and development of turbulent flow requires the characterisation of the apparently random fluctuations of fluid motion superimposed to the mean flow.

In the current paper characterisation of the airflow is assessed by applying hot film single sensor anemometry and two dimensional Particle Image Velocimetry (PIV) to simplified mechanical replicas representing different portions of the upper airway and different articulator positions. Articulator configurations associated with turbulent flow development are considered [8, 9]. Besides qualitative results a quantitative comparison between simulated and measured velocities is provided and discussed axisymmetrical free jet development.

2 Velocity field characterisation

Measured velocity data are required in order to validate velocity field simulations and in order to estimate fluid mechanical and acoustical relevant quantities by means of integration or differentiation. In the following quantities of interest are outlined. Next the case of the round free jet is considered. Finally the limitations due to single sensor anemometry scanning and two-component PIV are briefly considered.

2.1 Quantities of interest

For incompressible flows $\nabla \mathbf{U} = 0$ holds where $\mathbf{U} = (U, V, W)$ denotes the velocity vector. In this case the Navier-Stokes equations can be rewritten in terms of the vorticity $\omega$ as:

$$\frac{\partial \omega}{\partial t} + U \nabla \omega = \omega \nabla U + \nu \nabla^2 \omega \tag{1}$$

where $\nu$ denotes the kinematic viscosity. Hence estimation of the vorticity field yields an important fluid mechanical quantity. The full velocity gradient tensor $G$ is given as:

$$G = \frac{d\mathbf{U}}{d\mathbf{X}} = \begin{bmatrix} \frac{\partial U}{\partial x} & \frac{\partial U}{\partial y} & \frac{\partial U}{\partial z} \\ \frac{\partial V}{\partial x} & \frac{\partial V}{\partial y} & \frac{\partial V}{\partial z} \\ \frac{\partial W}{\partial x} & \frac{\partial W}{\partial y} & \frac{\partial W}{\partial z} \end{bmatrix}, \tag{2}$$

with $\mathbf{X} = (x, y, z)$ the position vector. The deformation tensor of eq. 2 can be decomposed into a symmetric...
part and an antisymmetric part:
\[
\frac{d\mathbf{U}}{dt} = \left[ \begin{array}{c}
\frac{\partial U}{\partial x} + \frac{1}{2} \left( \frac{\partial V}{\partial x} + \frac{\partial U}{\partial y} \right) \\
0 \\
\frac{\partial W}{\partial x} + \frac{1}{2} \left( \frac{\partial V}{\partial y} - \frac{\partial W}{\partial z} \right) \\
\frac{\partial W}{\partial y} + \frac{1}{2} \left( \frac{\partial V}{\partial z} - \frac{\partial W}{\partial x} \right)
\end{array} \right] + \left[ \begin{array}{c}
\frac{1}{2} \left( \frac{\partial V}{\partial x} + \frac{\partial W}{\partial y} \right) \\
\frac{1}{2} \left( \frac{\partial V}{\partial y} - \frac{\partial W}{\partial z} \right) \\
\frac{1}{2} \left( \frac{\partial V}{\partial z} - \frac{\partial W}{\partial x} \right) \\
0
\end{array} \right].
\]

The symmetric part represents the strain tensor with the elongational strains on the diagonal and the shearing strains on the off-diagonal, whereas the antisymmetric part contains only vorticity components. Hence eq. 2 can be expressed as:
\[
\frac{d\mathbf{U}}{dt} = \mathbf{D}(\mathbf{U}) + \frac{1}{\rho} \mathbf{S}(\mathbf{U}),
\]

where the term \(\mathbf{D}(\mathbf{U})\) denotes the Reynolds stresses. Together with the Poisson equation for \((p)\),
\[
-\frac{1}{\rho} \nabla^2 (U_j) = \frac{\partial (U_i)}{\partial x_i} \frac{\partial (U_j)}{\partial x_i} + \frac{\partial^2 (u_{ij})}{\partial x_i \partial x_j},
\]
the Reynolds equations provides 4 equations for the four unknowns \((\mathbf{U}), (p)\) and in addition the unknown Reynolds stresses. Therefore the set of equations is unclosed. The diagonal components of the symmetric Reynolds stress tensor \(\langle u_{ij}\rangle\),
\[
\langle u_{ij}\rangle = \left[ \begin{array}{ccc}
\langle u_1^2 \rangle & \langle u_1 u_2 \rangle & \langle u_1 u_3 \rangle \\
\langle u_1 u_2 \rangle & \langle u_2^2 \rangle & \langle u_2 u_3 \rangle \\
\langle u_1 u_3 \rangle & \langle u_2 u_3 \rangle & \langle u_3^2 \rangle
\end{array} \right],
\]
are normal stresses whereas the off-diagonal components are shear stresses. Half the trace of the Reynolds stress tensor defines the turbulent kinetic energy \(k(X, t)\):
\[
k(X, t) \equiv \frac{1}{2} \mathbf{u} \cdot \mathbf{u} - \frac{1}{2} \langle u_{ij} \rangle.
\]
So, obviously the Reynolds stresses are an important physical quantity appearing among others in Lighthill's stress tensor whose elements \(T_{ij}\) reduces for an inviscid and isentropic flow to
\[
T_{ij} = \rho \langle u_{ij} \rangle.
\]

2.2 Round free jet

The turbulent round free jet at the exit of a circular tube with length \(L\) and diameter \(d\) is characterised by self-similar behaviour of the mean velocity field as well as the Reynolds stresses [7]. The mean centerline velocity \(U_c(x)\) is expected to decrease proportional to \(x^{-1}\) while the mean radial profiles \(U(x, y)\) scales with the centerline velocity:
\[
\frac{U_0}{U_c} = \frac{1}{K} \frac{x - x_0}{d} \quad \text{and} \quad \frac{U(x, y)}{U_c(x)} = e^{-\alpha y^2}
\]
with \(K\) centerline decay rate, \(\eta = \frac{x}{d}, U_0\) the velocity at the tube exit, \(x_0\) virtual origin, \(x\) the flow direction, \(y\) the transverse radial direction and the model parameter \(\alpha\) derived from the radial spreading rate \(S\) as \(\alpha = \ln(2)/S^2\) often yielding \(\alpha = 94\) for a round free jet. Besides the mean velocity field the turbulence statistics expressed by root mean square (rms) \(u' = \sigma = \langle u^2 \rangle^{1/2}\) and higher moments, i.e. skewness \(S_u = \langle u^3 \rangle / \sigma^3\) and kurtosis \(K = \langle u^4 \rangle / \sigma^4\), approach Gaussian values in the self-similar region.

A turbulent viscosity \(\nu_T(x, y) = y_{1/2} U_c(x) \tilde{\nu}_T(\eta)\) can be estimated from \(S\) and jet half width \(y_{1/2}\) as
\[
\nu_T(x, y) = y_{1/2} U_c(x) \tilde{\nu}_T(\eta) \quad \text{with} \quad \tilde{\nu}_T(\eta) = \frac{S}{8(\sqrt{2} - 1)}.
\]
The assumption of turbulent viscosity \(\nu_T(x, t)\) allows to overcome the closure problem and to estimate the shear stress from the mean velocity field,
\[
\langle u_1 u_2 \rangle = - \nu_T \frac{\partial (U_1)}{\partial r}.
\]
The Reynolds stress tensor for a two-dimensional flow statistically invariant under reflections of the \(z\) coordinate axis reduces to
\[
\langle u_{ij} \rangle = \left[ \begin{array}{ccc}
\langle u_1^2 \rangle & \langle u_1 u_2 \rangle & 0 \\
\langle u_1 u_2 \rangle & \langle u_2^2 \rangle & 0 \\
0 & 0 & \langle u_3^2 \rangle
\end{array} \right].
\]
Furthermore the velocity spectra inform on the energy scales. A simple power law is applied in order to model the energy spectra \(E(k)\) as:
\[
E(k) = \frac{C_1}{(1 + \frac{k}{k_0})^\gamma}.
\]
with wavenumber \(k\) and \(C_{1,2}\) model constants. Exponent \(n\) set to \(n = 5/3\) and \(n = 3\) corresponds to Kolmogorovs and Kraichmans law respectively indicating the inertial and decay portion of the spectra respectively [4].

2.3 Measurement limitations

Single sensor or one-component (1D) anemometry or two-component PIV (2D PIV) provides at most the \(x\) and \(y\) velocity components. Consequently this data can only be differentiated with respect to the \(x\) and \(y\) directions. Therefore only a few terms of the deformation tensor, eq. 4, can be estimated, i.e. vorticity component \(\omega_z\), normal to the light sheet in case of 2D PIV along with the in-plane shearing \(\epsilon_{xy}\) and extensional strains \(\epsilon_{xx}\) and \(\epsilon_{yy}\). Remark that for an incompressible flow, \(\nabla \cdot \mathbf{U} = 0\), the third in-plane extensional strain can be estimated as \(\epsilon_{zz} = -(\epsilon_{xx} + \epsilon_{yy})\). Following [10] vortices appear
for non-real eigenvalues of the reduced velocity gradient tensor $\mathcal{G}$:

$$\mathcal{G} = \frac{\partial U}{\partial x} = \begin{bmatrix} \frac{\partial U}{\partial x} & \frac{\partial V}{\partial x} \\ \frac{\partial U}{\partial y} & \frac{\partial V}{\partial y} \end{bmatrix}. \quad (16)$$

The discriminant $\lambda_2$ of non-real eigenvalues of the velocity tensor $\mathcal{G}$ separates vortices from other patterns:

$$\lambda_2 = (\text{trace } \mathcal{G})^2 - 4 \det (\mathcal{G}) \quad (17)$$

3 Experimental setup

Qualitative and quantitative characterisation of the instantaneous velocity field is experimentally assessed with 1D anemometry and 2D PIV [5, 1]. PIV has the advantage to inform non-intrusively on large parts of flow fields while anemometry allows direct measurement of the velocity distribution. Mechanical ‘in-vitro’ replicas with different degree of complexity and typical airflow conditions encountered during speech production are briefly described in the next section.

3.1 Experimental conditions

The upper airway geometry stretches from the larynx up to the lips as depicted in Fig. 1. Airflow conditions in the upper airways during speech production are characterised in terms of relevant non-dimensional numbers as: Reynolds $Re \approx O(10^3)$, Mach $Ma \approx O(10^{-2})$, Strouhal $Sr \approx O(10^{-2})$ and the airflow is assumed to be incompressible [6, 9]. The vocal tract length ranges from 7 up to 18 cm depending on age and morphology whereas position and degree of constrictions depend on the articulators configuration. Rigid and deformable ‘in-vitro’ mechanical replicas with different degree of complexity are developed in order to study the flow behaviour and the influence of mechanical conditions, e.g. [2, 3, 6]. In the following severely simplified rigid and deformable replicas are considered as illustrated in Fig. 2 [6, 2].

![Figure 2: Schematic overview of some ‘in-vitro’ geometries: circular tube, exemplary rigid downstream constrictions with or without forced movement (y dimension), front view deformable replica.](image)

3.2 Single sensor anemometry

A jet is generated in a flow facility consisting of an air compressor (Atlas Copco GA7) followed by a manual valve and pressure regulator (Norgren type 11-818-987) enabling to provide constant air pressure. A constant temperature anemometer system (IFA 300) is available in order to perform flow velocity measurements. The hot-film is calibrated against mean velocities given by the flow meter. A fourth polynomial law is fitted to the anemometer output voltage in order to convert measured voltage to velocity with an accuracy of 0.1m/s. Longitudinal ($x$) and radial ($y$) velocity profiles are obtained by moving a single sensor hot film (TSI 1201-20) with a diameter of 50.8µm and a working length of 1.02mm using a two-dimensional stage positioning system (Chuo precision industrial co. CAT-C, ALS-250-C2P and ALS-115-E1P) with accuracy $\Delta x = 4$ and $\Delta y = 2\mu m$. At each position velocity data are acquired at 30kHz for 3s consecutively.

3.3 Two component PIV (2D PIV)

Smoke tracer particles with a mean diameter inferior to 1µm are added to the airflow. A plane within the flow is illuminated twice by means of a laser (dual-YAG) light sheet whereas the time delay is adapted depending on the mean flow velocity and the magnification of imaging. It is assumed that the flow particles move with local flow velocity between the two illuminations. The light scattered by the tracer particles is recorded on a single frame (Lavision camera with 1376×1024 pixels). The local displacement vector is determined for each interrogation area by means of statistical methods relating on correlation analysis with commercial software (Lavision Davis 7). It is assumed that all particles within one interrogation area have moved homogeneously between the two illuminations. The projection of the vector of the local flow velocity into the plane of the light sheet resulting in the two-component velocity vector is calculated taking into account the time delay between the two illuminations and the magnification at imaging.

4 Results and discussion

4.1 1D anemometry of round free jet

An axisymmetrical free jet issuing from a uniform circular extension tube as depicted in Fig. 2 with diameter $d=25mm$ and varying length $L_t$ is considered where the subscript $t$ denotes the tube length in cm. The time averaged spatial velocity development is scanned with 1D anemometry mounted on a positioning system as outlined in section 3.2. The assessed extension tube lengths yield 1, 3, 9, 18 and 50cm corresponding to $L_t/d \in \{0.4, 1.2, 3.6, 7.2, 20\}$. Longitudinal data along the $x$ direction are gathered from the tube exit up to 20$d$. Radial profiles along the $y$ direction are assessed near the tube exit and at 1.6, 3.2, 4, 4.8, 6.4, 8, 12 and 16$d$. Varying the tube length $L_t$ is a simple way to assess the influence of initial conditions corresponding to aging or articulation on the self-similar spatial jet development for a fixed volume flow rate of 130l/min or $U_b=4.4m/s$ corresponding to $Re \approx 7350$. Exemplary time averaged statistics derived from the measured instantaneous velocity data are presented in Fig. 3. The mean longitudinal velocity profiles and exemplary mean radial velocity profile at $x=3.2d$ are illustrated in Fig. 3(a) and 3(d). Both mean profiles prevail self-similarity as expressed in eq. 11 although the centerline decay constant $K$ and model parameter $\alpha$ are seen to depend on $L_t/d$ as shown in Fig. 4 for $K(L_t/d)$. The influence
of \(L_i/d\) on initial conditions is illustrated in Fig. 3(b) for the mean and in 3(f) for the fluctuating part of the velocity. Except for \(L_i=1\)cm the initial mean velocity profile approaches Blasius solution \(U/U_c = (1 - 2y/d)^{1/7}\) with \(n = 7\) when \(L_i/d\) increases. The turbulence level at the exit increases from about 10 up to 60% of the centreline exit velocity when \(L_i/d\) is increased. The fluctuating centerline velocity can be characterised by its higher moments as illustrated for the centerline skewness in Fig. 3(c). The higher moments converge towards a constant value away from the exit for all assessed \(L_i/d\). Moreover in the self-similar region this constant value approaches the value expected for a Gaussian distribution. The distance \(x/d\) needed to reach this constant value increases with \(L_i/d\) in consequence with the decreasing initial turbulence level. Moreover Gaussian values are seen to fit in particular for larger \(L_i/d\). In accordance with the initial profiles the turbulence level decreases when \(L_i/d\) increases in the radial rms profiles as illustrated in Fig. 3(d). For the two smallest \(L_i/d\) the flow is turbulent from the exit, while for the larger \(L_i/d\) development of the shear layers is observed. The measured data are in agreement with the higher moments and mean centerline velocities indicating the absence of a potential cone for the smallest tube lengths \(L_i/d\). A turbulent viscosity can be estimated for the flow following Eq. 12 from which the shear stress \((u_1 u_2)\) is derived as in eq. 13. From the exemplar shear stresses shown in Fig. 3(g) is seen that although the overall shape is the same, \(L_i/d\) and hence initial conditions influences the resulting shear stresses in several ways concerning the position, amplitude and width of the two peaks and as a consequence the slope between both peaks in accordance with the changes in \(\nu_T/S\) causing a stretching of the shear stresses. The one dimensional velocity spectra \(P_u(k)\) at \(x = 1.6d\) and maximum shear stress position \(y/d \approx 0.7\) is illustrated in Fig. 3(h) for dimensionless wavenumber \(k = \omega.d/U_c(x)\). As for the shear stress the general shape is seen to be similar for all assessed \(L_i/d\). The energy spectra are modelled following eq. 15 with \(C_2 = 0.07\) for all spatial positions and all assessed \(L_i/d\) whereas \(C_1\) varies with spatial position. Kolgomorovs power law \(E(k) \sim k^{-5/3}\) describes well the inertial part of the spectrum while Kraichnans power law \(E(k) \sim k^{-\alpha}\) is seen to match the decay part. Hence the energy scales can be derived. Although in particular concerning the decay part a fine analysis reveals a faster decay for large \(L_i/d\) compared to small \(L_i/d\) and the same way the decay onset appears for slightly lower \(k\)-values for large \(L_i/d\) as for small \(L_i/d\).

### 4.2 2D PIV

The characterisation presented in the previous section concerning a round free jet can be assessed in case 2D PIV data are considered. Resulting mean and rms are illustrated in Fig. 5 for a jet issuing from a circular tube with \(d=25\)mm as before, \(L_i/d=8.8\) and \(Re \approx 20000\). The flow through typical configurations of ‘in-vitro’ replicas depicted in Fig. 2 or ‘in-vivo’ articulator config-
The support of the French Rhône-Alpes Region (CIBLE 2006) and Agence National de la Recherche (ANR-07-JCJC-005) is gratefully acknowledged. Thanks for technical support at LEA: Laurent Philippon, Pascal Biais and Patrick Braud.

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